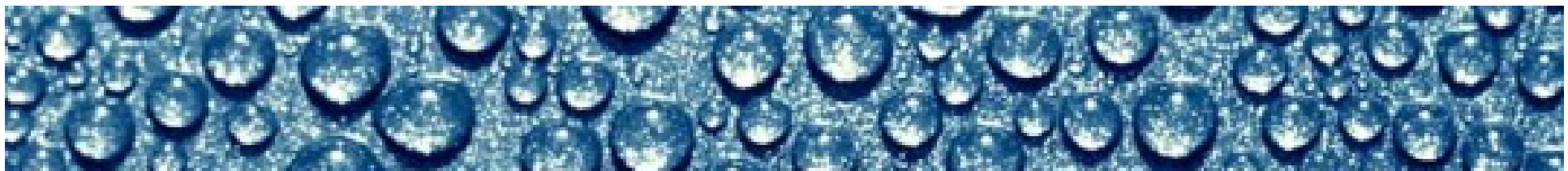


# **Wet Gas Performance of Coriolis Meters: Lab and Field Results**

**by**

**Justin Hollingsworth  
Emerson Automation Solutions**



# Agenda

**Introduction**

**Quick Coriolis Overview**

**Design Elements to Consider for Multiphase Use**

**Determination of Multiphase Conditions**

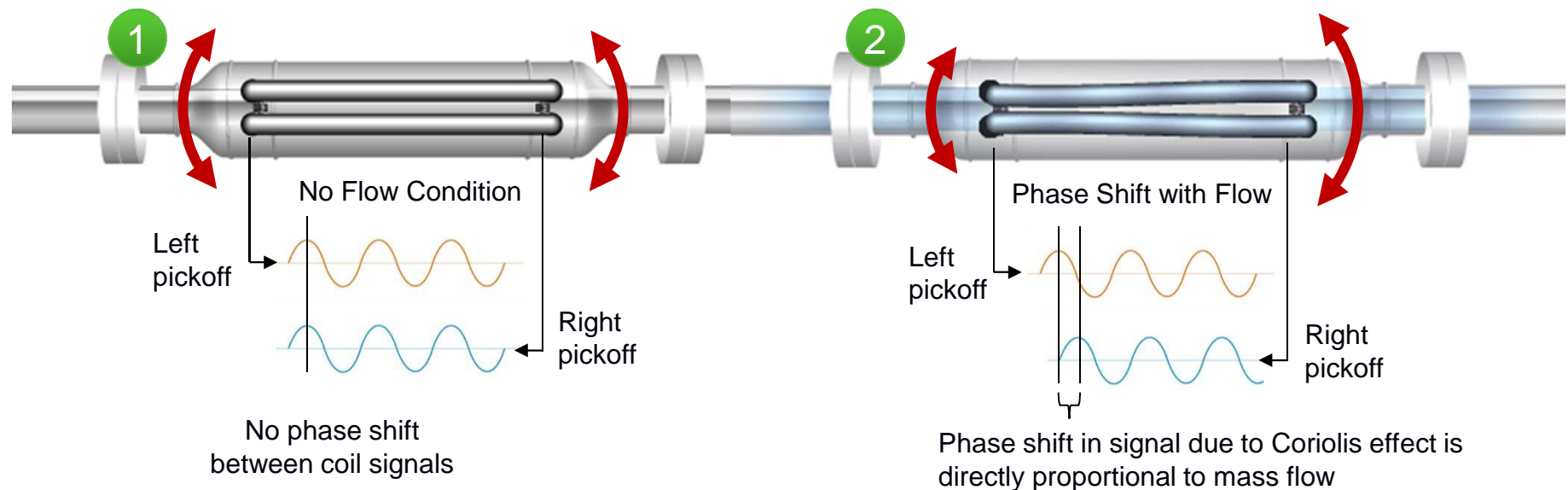
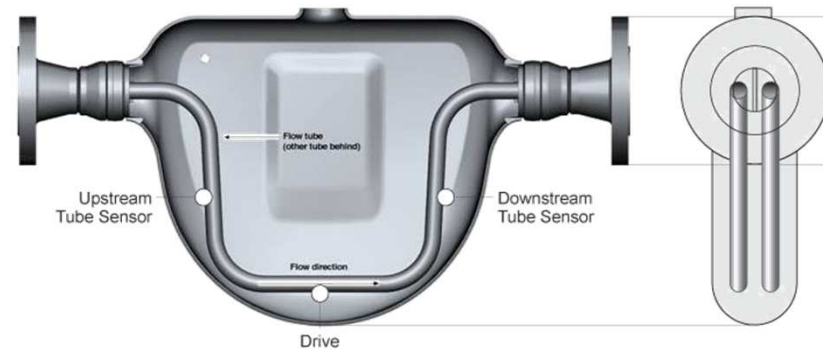
**Algorithms for Different Flow Regimes**

**Results from Testing in Lab and Field**

**Conclusion**

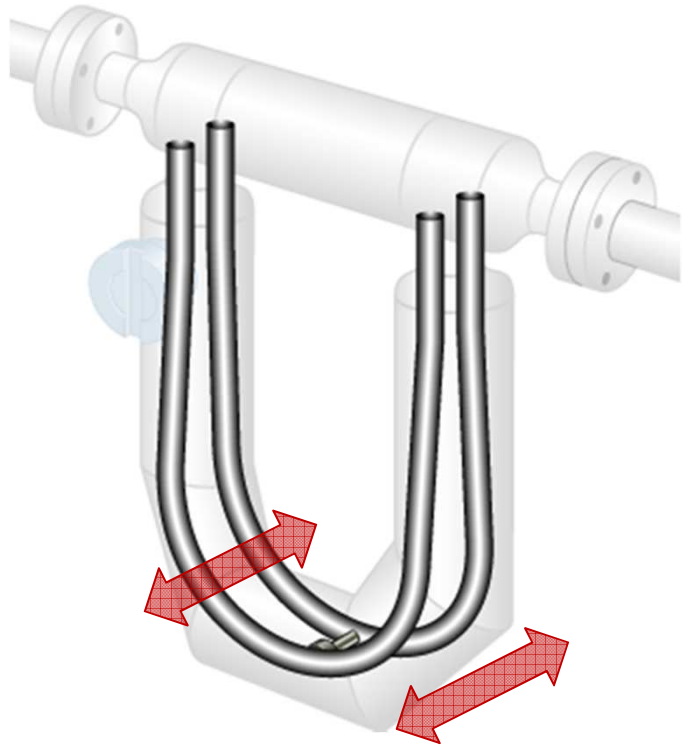
# Theory of Operation – The Coriolis Effect

- 1 During a no flow condition, flow tubes vibrate in phase with each other.
- 2 With flow, Coriolis forces are induced causing the flow tubes to twist in opposition to each other.

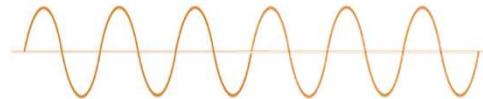


**Phase shift between pickoff coils is directly proportional to mass flow**

# Theory of Operation - Density



Low Fluid Density *decreases* system mass and *increases* frequency of tube oscillation



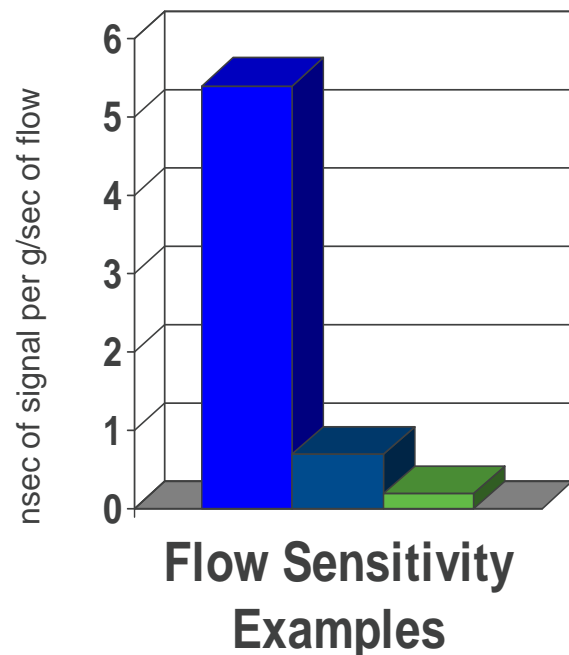
High Fluid Density *increases* system mass and *decreases* frequency of tube oscillation



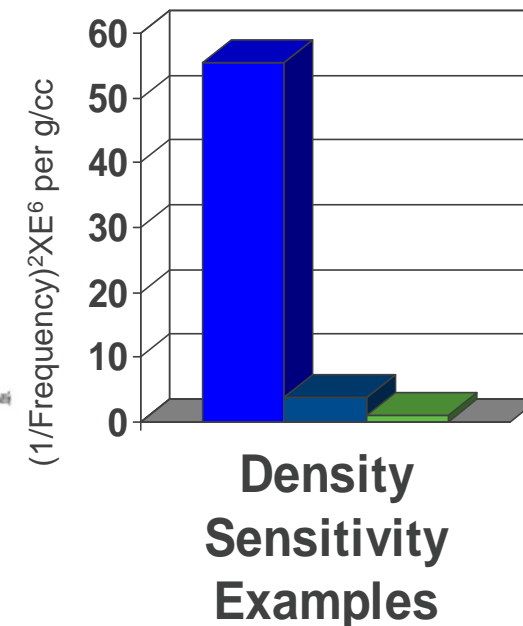
**Density measurement is based on the natural frequency of the system, including the flow tubes and the process fluid.**

# Coriolis Meter Raw Sensitivity Varies with Design

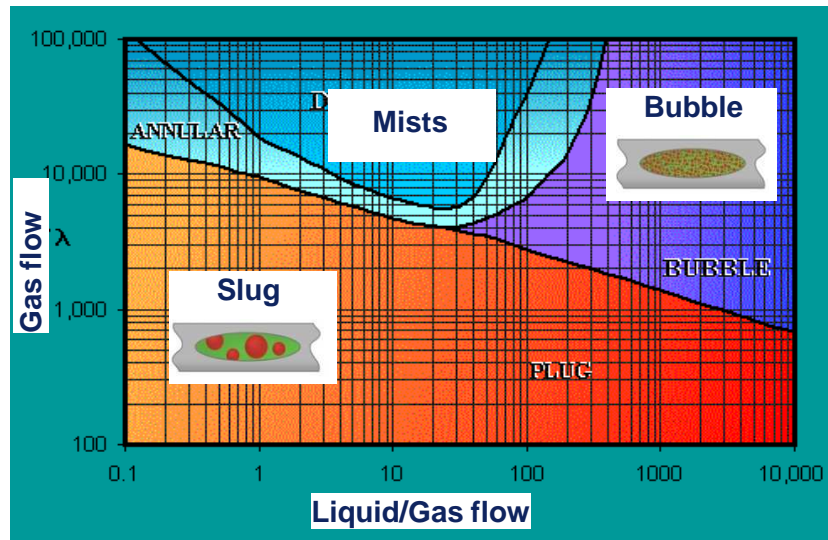
- **Raw Sensitivity Depends on Tube Geometry**
- **Signal to Noise Ratio Depends on Raw Sensitivity and Stability**
- **Accuracy, Stability, Calibration Flexibility, Immunity to Secondary Effects, and Diagnostic Capabilities Depend on Signal to Noise Ratio**



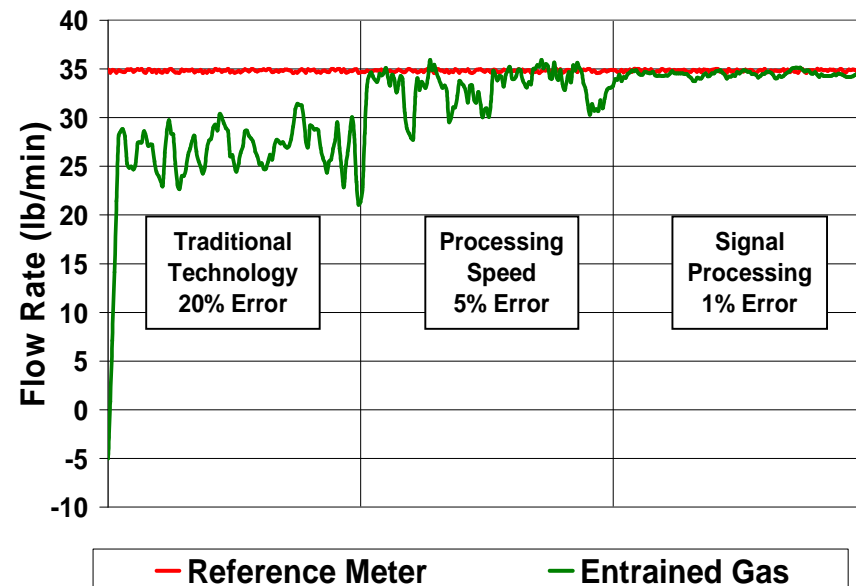
■ Tall Tube Geometry  
■ Medium Tube Geometry  
■ Short Tube Geometry



# Improvements to Handle Entrained Gas



**MVD**™ technology



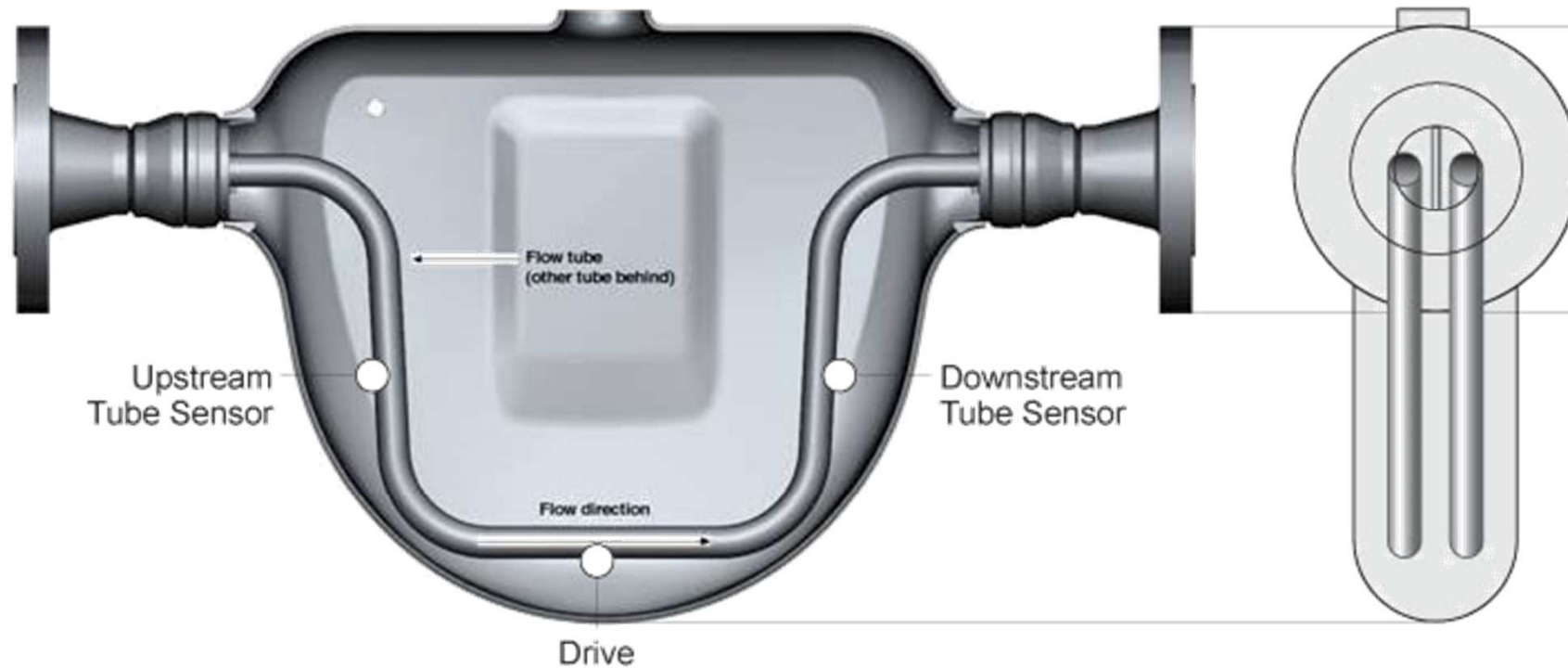
## Electronics Improvements

- Processing speed
- Signal processing algorithms
- Function with noisy signals

## Structure Improvements

- Better balance and vibration isolation
- Modal separation

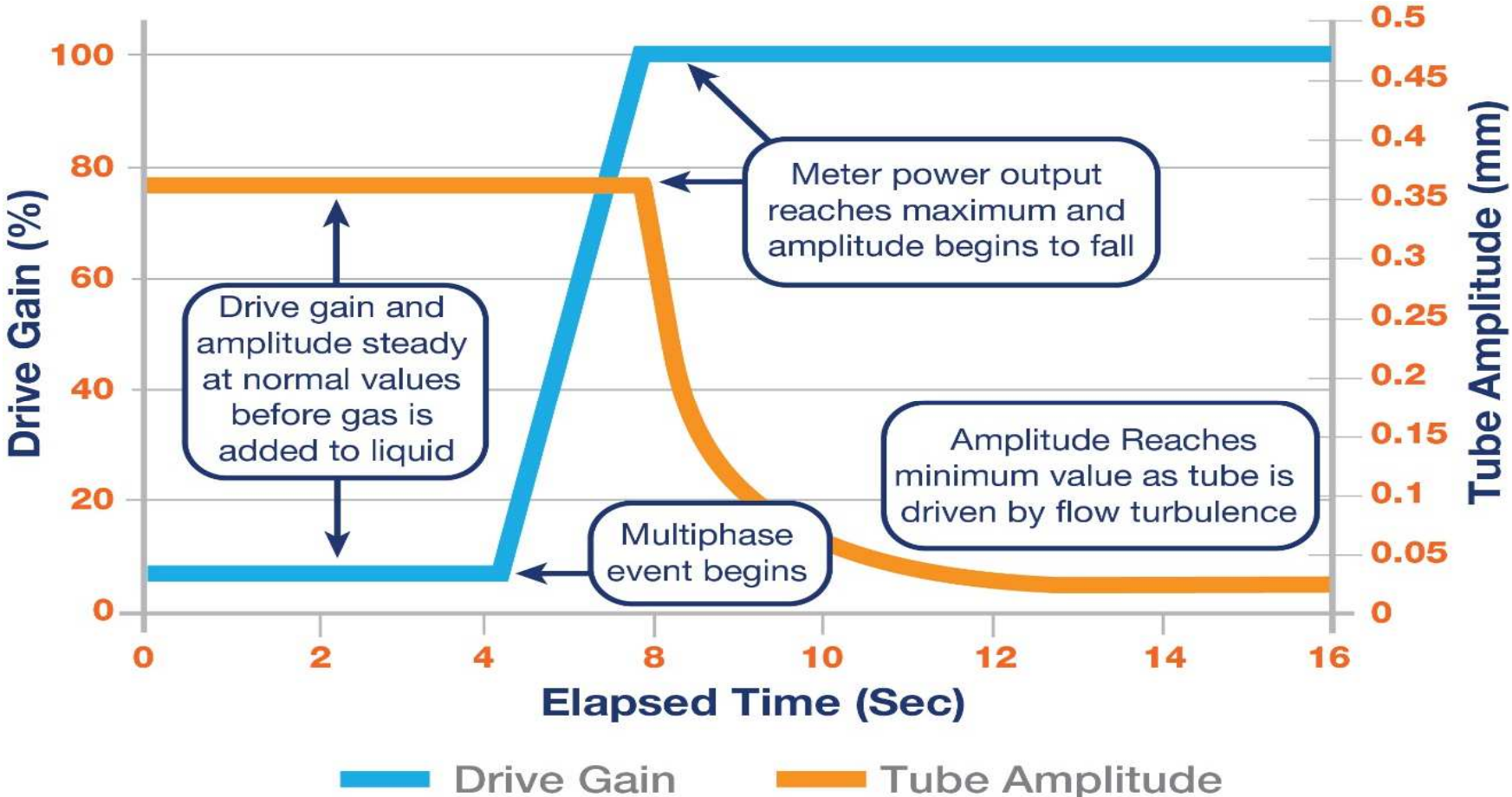
# Vibration Drive and Amplitude



**Drive and pickoff coils provide damping data**



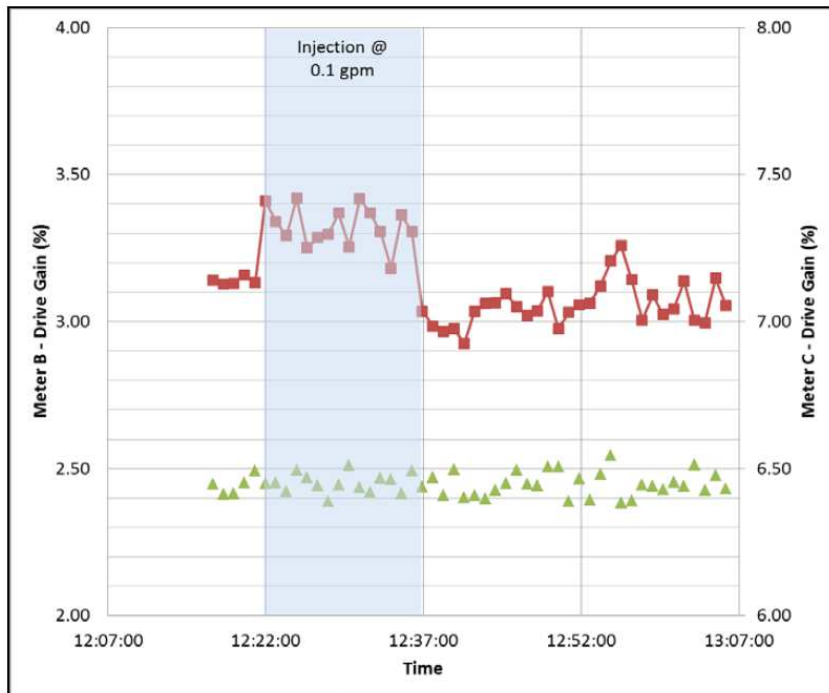
# Detection of Multiple Phases



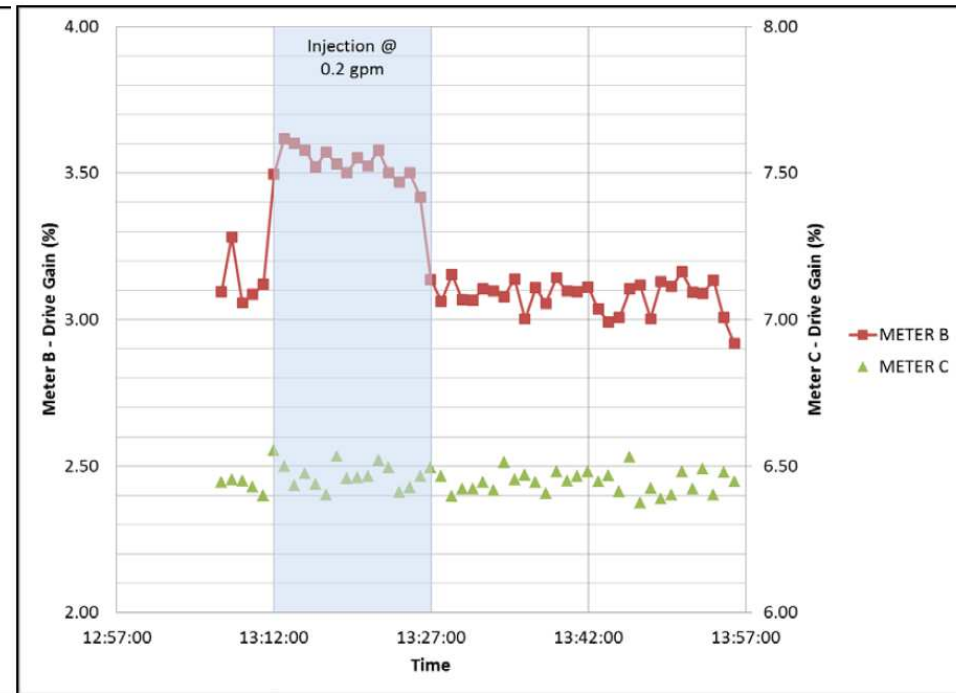
**Damping of flow tubes indicates multiple phases**



# Identification of Mist: 99.9+% GVF



Drive Gain Results for Meter B at 100 acfm and 0.1 gpm



Drive Gain Results for Meter B at 100 acfm and 0.2 gpm

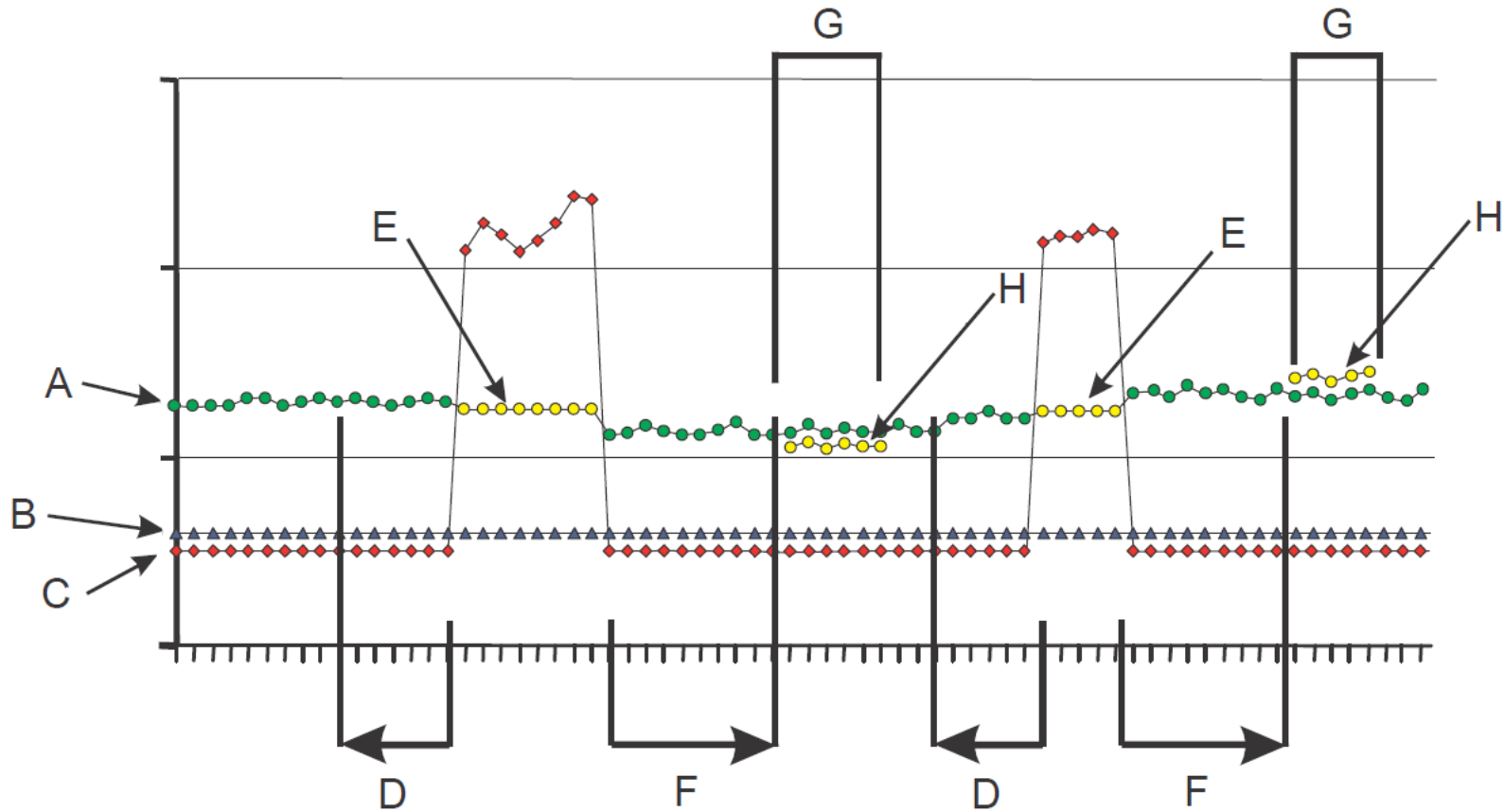
**Sensor element design, signal processing and control of vibration has effect on ability to detect phase contamination**

# Algorithm for Slugging Regime & Intermittent Multiphase

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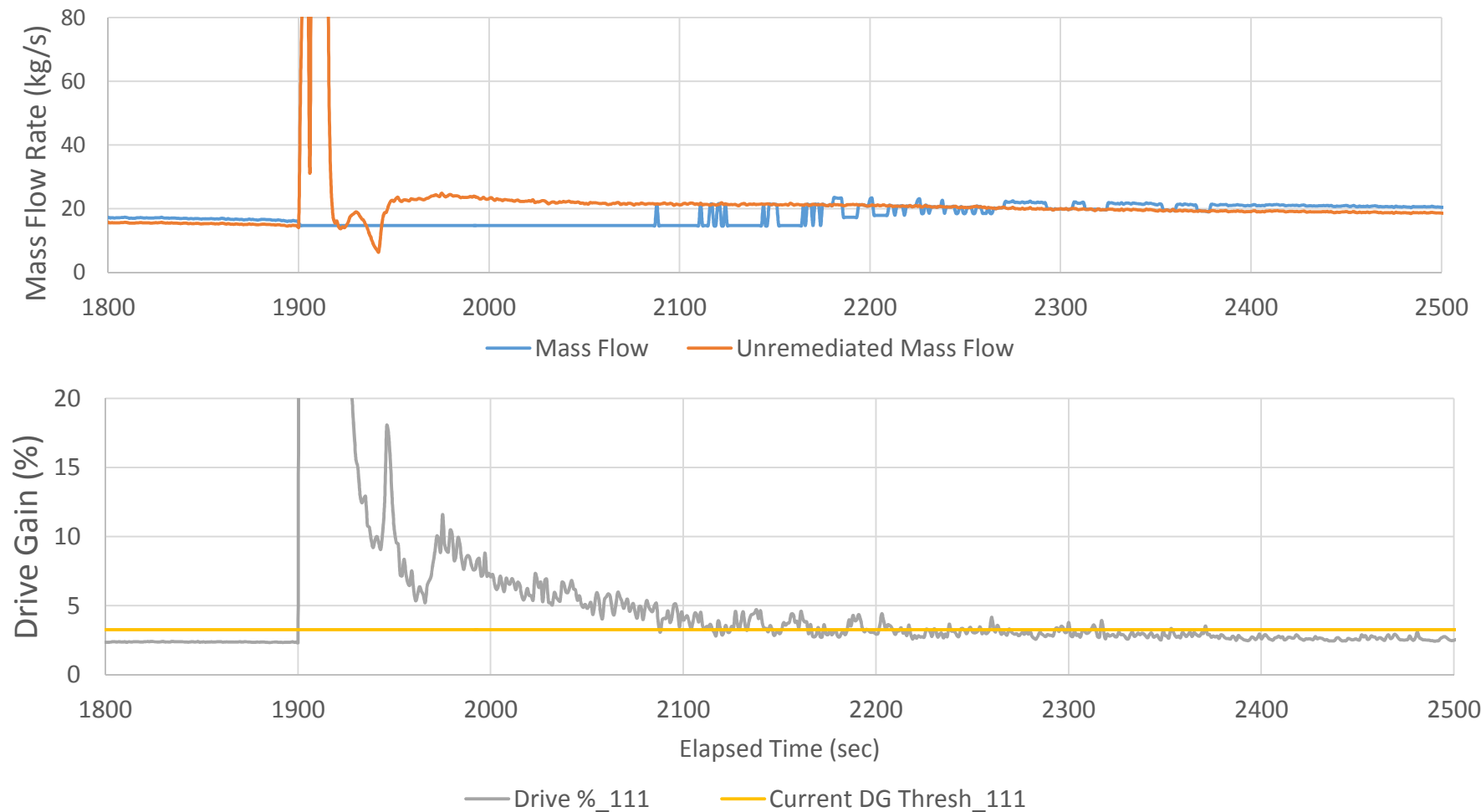
- Tube damping provides very sensitive detection, but it is not a measurement of phase fraction
  - With this diagnostic, we can break up the wet gas problem into
    - Unstable or intermittent wet gas – the process is normally dry, but there are slugs or occasional phase contamination
      - This has several real world applications: separators, plunger lift, etc.
    - Stable or continuous wet gas.

# Simple Wet Gas Algorithm



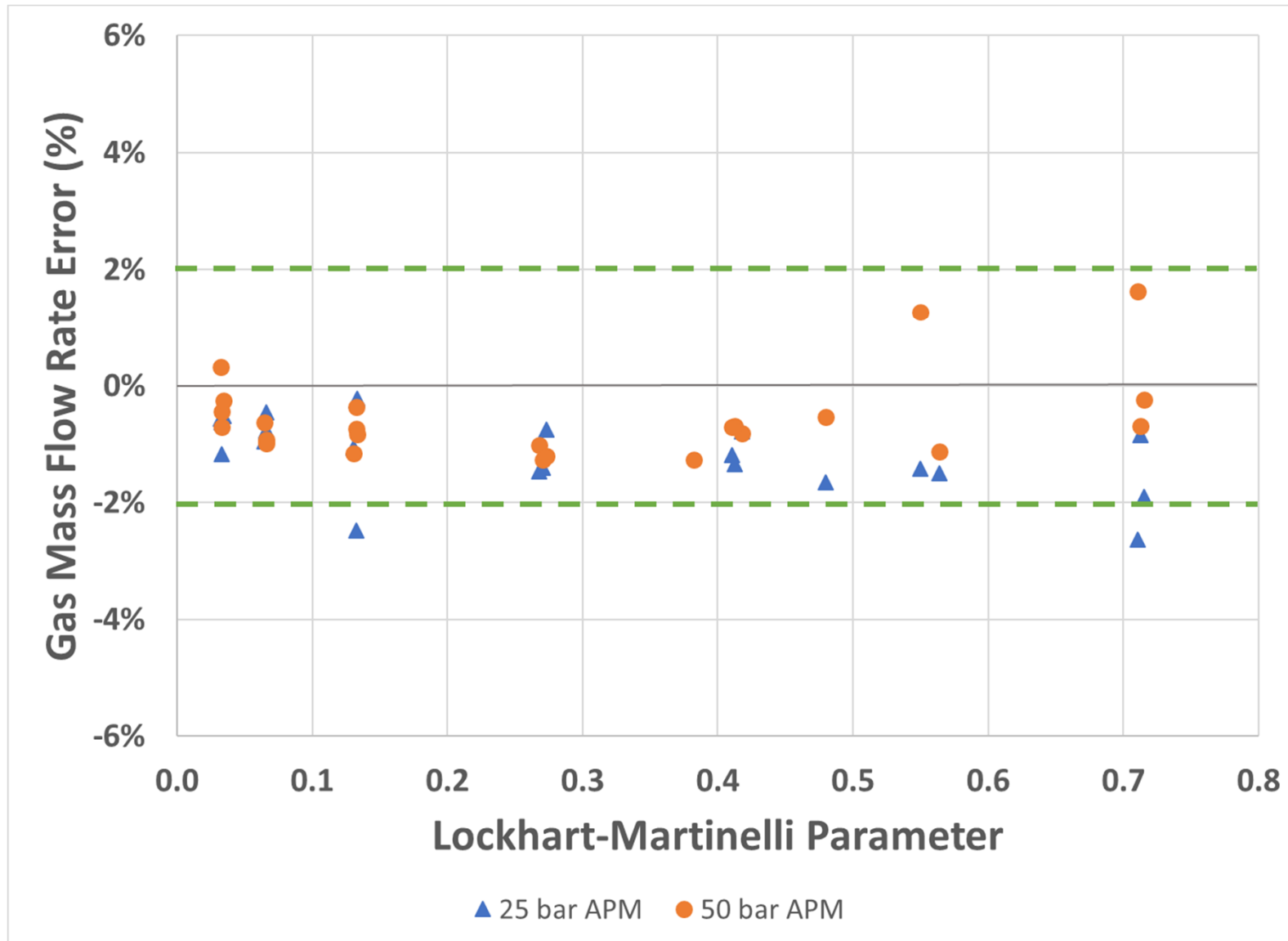
- A. Flow rate
- B. TMR Drive Gain Threshold
- C. Drive gain (actual)
- D. Pre-Mist Averaging Period and source of M1
- E. Averaged flow rate values
- F. Post-Mist Adjustment Delay and source of M2
- G. Adjustment period
- H. Adjusted flow rate values

# Algorithm for liquid slugs in gas



**Immediate detection of liquid slugs allows them to be excluded from gas measurement**

# CEESI Testing – Slugging Regime



# Method for Stable Wet Gas

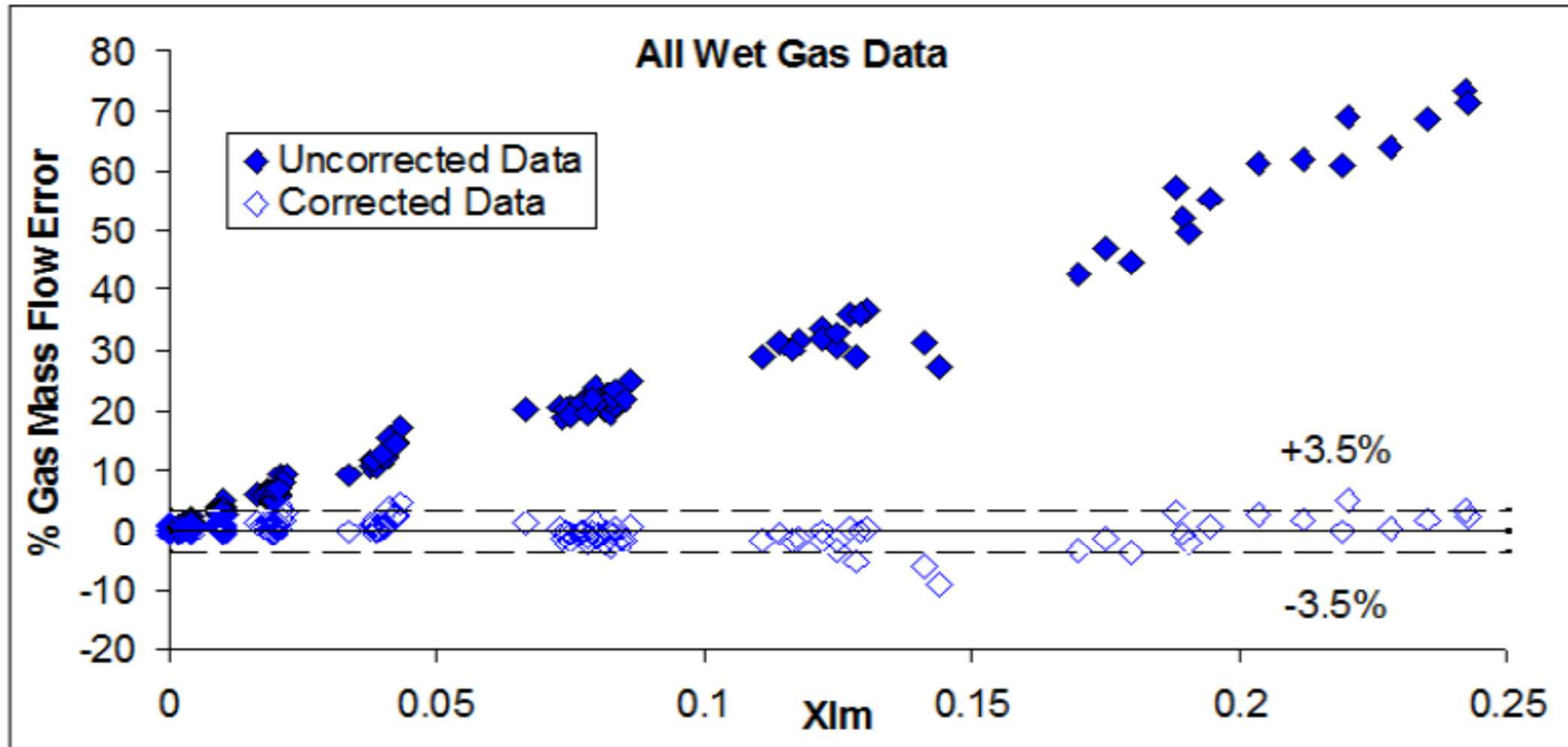
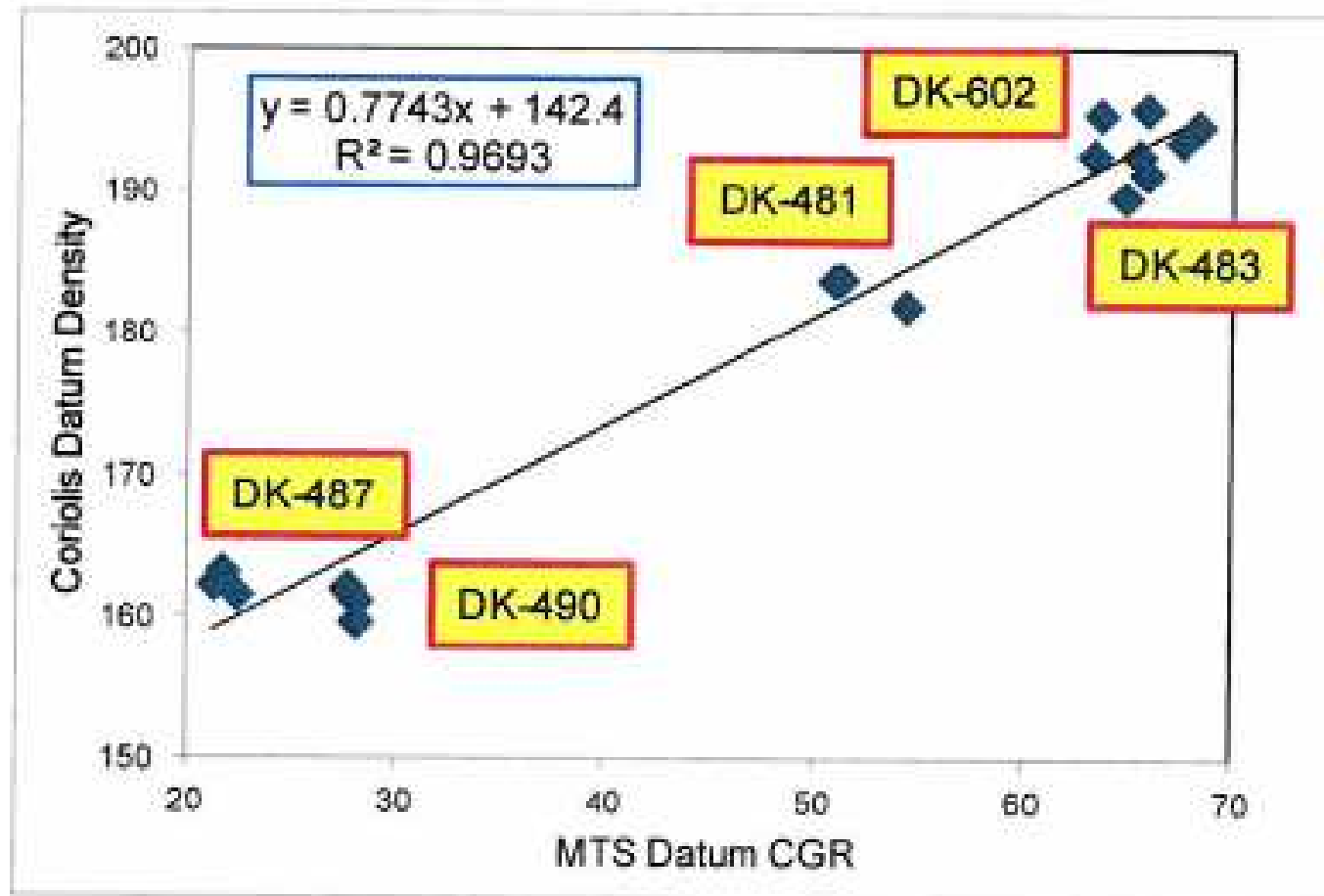


Fig. 16 - 3" Coriolis Meter Over-Reading vs. XLM Uncorrected & Corrected Data.

Richard Steven and Josh Kinney (CEESI), "Coriolis Meters & Wet Gas Service," In Proc. *South East Asia Flow Measurement Conference 2017*

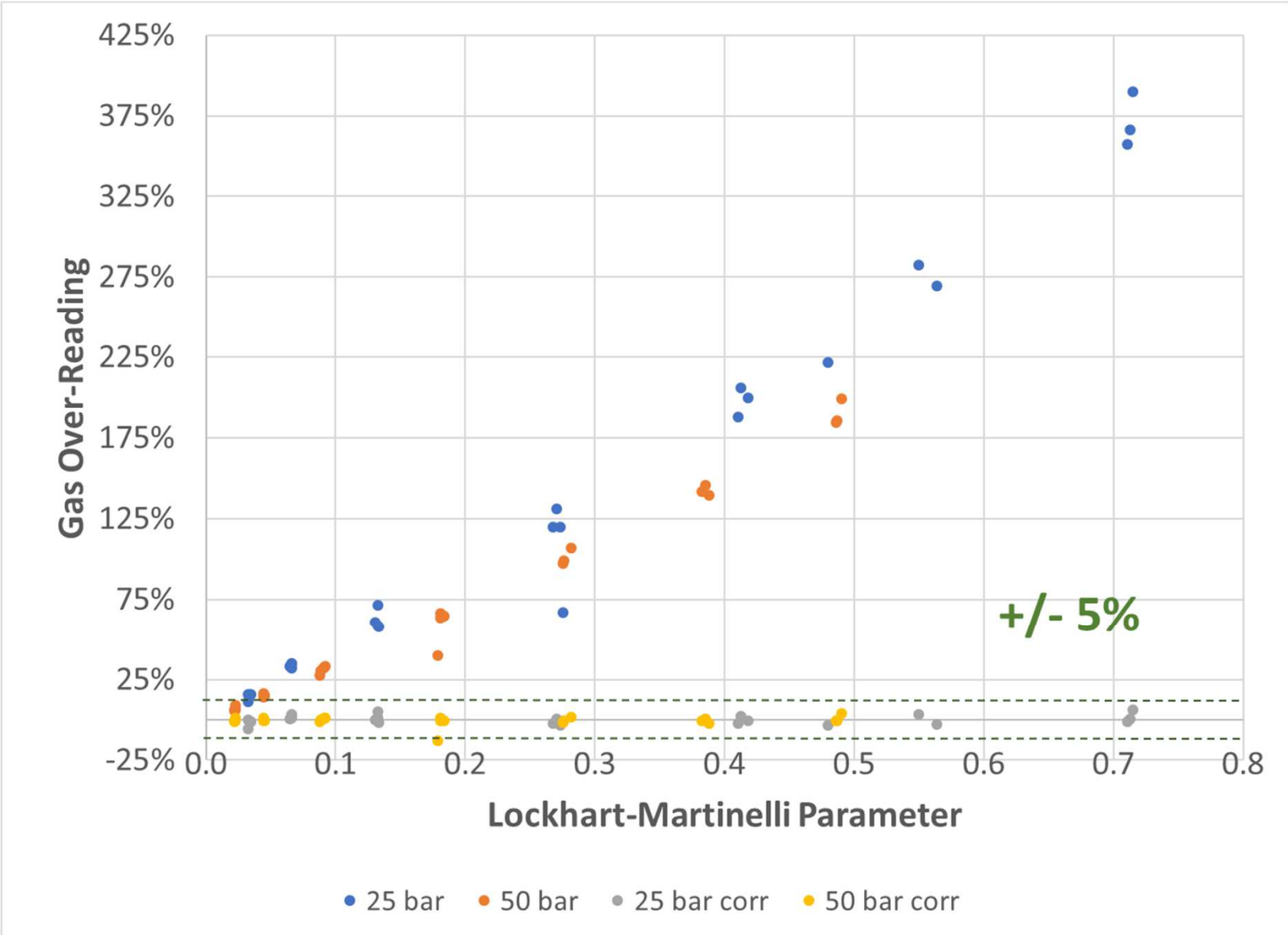
# Simple Approach to Density Reference



**A useable approach in the field is to use well tests to reference measured density to phase fractions**



# Extending Corrections for More Liquid



# Experience in the Field

- Field conditions always more challenging than lab
  - Different process conditions, fluid properties, hydrates, solids
  - Installation issues
  - Questionable references
- Thousands of meters in the field using intermittent multiphase algorithm
  - Separator outlets, plunger lift wells, naturally slugging regimes
  - Generally accepted to be within  $\pm 3\%$  GSV over broad range of pressure, temperature, flow rate and liquid loading conditions
- Multiple field trials underway on continuous / changing regime wet gas
  - Initial results within uncertainty of field reference:  $\pm 7\%$  GSV
  - Primary challenge is hydrate formation
  - Tracking field operational changes that could affect trial also a challenge

# Summary

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- Coriolis technology has improved in the past 10 - 20 years
  - Time to revisit guidelines for wet gas use
- Not all Coriolis designs are expected to have the same behavior in multiphase or wet gas
- It appears that viable methods exist to correct flow outputs, with knowledge of flow regime
  - May be less reliant on external inputs than existing approaches
  - Coriolis meters can provide regime data, depends on design
- Additional research needed, revisit guidance on coriolis suitability for wet gas applications
  - Need to address field implementation challenges